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<b>(21) International Application Number:</b> PCT/US94/09462 <b>(22) International Filing Date:</b> 26 August 1994 (26.08.94)  <b>(30) Priority Data:</b> 08/113,982 2 September 1993 (02.09.93) US  <b>(71) Applicant:</b> E.I. DU PONT DE NEMOURS AND COMPANY [US/US]; 1007 Market Street, Wilmington, DE 19898 (US).  <b>(72) Inventor:</b> DEAK, Gedeon, Imre; 14 Ravine Road, Wilmington, DE 19810-2932 (US).  <b>(74) Agents:</b> KAEDING, Konrad, S. et al.; E.I. Du Pont de Nemours and Company, Legal/Patent Records Center, 1007 Market Street, Wilmington, DE 19898 (US).		<b>(81) Designated States:</b> CA, European patent (AT, BE, CH, DE, DK, ES, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE).  <b>Published</b> <i>With international search report.</i> <i>Before the expiration of the time limit for amending the claims and to be republished in the event of the receipt of amendments.</i>
<b>(54) Title:</b> SOLUTION COATING PROCESS FOR PACKAGING FILM  <b>(57) Abstract</b>  A process for applying a barrier layer of ethylene/vinyl alcohol copolymer (EVOH) to a substrate, such as a plastic film, by coating the substrate with a solution of EVOH in a solvent of tetrahydrofuran and water, followed by removing the solvent and a coating solution is disclosed. Such coating solutions have lower viscosity than equally concentrated solutions of EVOH in alcohol-based solvents and have greater shelf lives than alcohol-based solutions. Multilayer structures having an EVOH barrier layer coated on a plastic substrate from solution in aqueous tetrahydrofuran solvent have excellent oxygen barrier properties.		

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## SOLUTION COATING PROCESS FOR PACKAGING FILM

BACKGROUND OF THE INVENTION

5 The present invention relates to solution coating barrier layers on plastic films.

The gas permeability of certain plastic articles, such as films, can be reduced by coating the article with a barrier material. Ethylene/vinyl alcohol copolymer (EVOH) is recognized as a barrier material which is especially good for reducing the permeability to oxygen. By coating  
10 plastic with an EVOH layer it is possible to make clear, strong film which is well suited for packaging oxygen-sensitive products such as food and chemicals.

One of many methods to apply polymer coatings to substrates is solution coating. Typically in such process, the coating material is  
15 dissolved in a convenient solvent, the solution is deposited on the film surface and thereafter the solvent is removed. Solution coating is advantageous for placing very thin coatings on sheets, films and substrates which have complex shapes such as containers. Generally, alcohols, and mixtures of alcohols with water, are preferred solvents for  
20 solution coating substrates with EVOH because they are inexpensive and have moderately low toxicity. Solutions of EVOH in alcohols, however, tend to gel or precipitate after short-term aging. Consequently, they have only limited shelf life. Furthermore, alcohol-based solutions of EVOH have high solution viscosities. Dilute  
25 solutions must be used in order to attain sufficiently low solution viscosity for proper coating process operation. Dilute solutions, however, are costly because of the large amount of solvent consumed and long drying time needed to remove the solvent. Use of dilute

solutions is also environmentally unattractive because of the need to recover large quantities of spent solvent.

### SUMMARY OF THE INVENTION

The present invention provides a process for solution coating  
5 barrier layers on substrates using concentrated, yet low viscosity and stable EVOH solutions in solvent of tetrahydrofuran and water.

Specifically, there is now provided a process for solution coating a substrate with an ethylene/vinyl alcohol copolymer (EVOH) barrier, comprising the steps of:

- 10 (1) agitating a coating solution consisting essentially of
    - (A) about 7 to about 20 wt% ethylene/vinyl alcohol copolymer having copolymerized ethylene content from about 20 to about 55 mole %; and
    - (B) a complementary amount to total to 100 wt% of a  
15 solvent consisting essentially of about 10 to about 70 wt% water; and a complementary amount to total 100 wt% of tetrahydrofuran;at a temperature within the range of about 55-100°C until a clear solution is obtained;
  - 20 (2) coating at least one surface of the substrate with the coating solution; and
  - 3) removing the solvent, whereby a dry ethylene/vinyl alcohol copolymer coating on the at least one surface is produced.
- There is further provided a coating solution consisting essentially of:
- 25 (A) about 7 to about 20 wt% ethylene/vinyl alcohol copolymer having copolymerized ethylene content from about 20 to about 55 mole %; and

(B) a complementary amount to total 100 wt% of a solvent consisting essentially of about 10 to about 70 wt% water; and a complementary amount to total 100 wt%, of tetrahydrofuran.

#### **BRIEF DESCRIPTION OF THE DRAWINGS**

5 The figure is a side elevation view of a continuous, doctor roll coating system for solution coating one side of a film.

#### **DESCRIPTION OF THE PREFERRED EMBODIMENTS**

Definition: The term "consisting essentially of" means that other materials than ethylene/vinyl alcohol copolymer, tetrahydrofuran and  
10 water can be present in solution; provided that such other materials do not detract from the operability of the present invention.

The principal component of the solution of the present invention is ethylene/vinyl alcohol copolymer (EVOH). EVOH useful in this invention includes resins having a copolymerized ethylene content of  
15 about 20 to about 55 mole%, especially about 25 to about 50 mole %. Copolymers of higher than about 55 mole % ethylene tend to have reduced gas barrier performance. These copolymers will have a saponification degree of at least about 90%, preferably at least about 95%, and more preferably at least about 99%. A degree of  
20 saponification of less than about 90% results in inferior gas barrier properties. The EVOH may include as an optional comonomer other olefins such as, for example, propylene, 1-butene, 1-pentene and 4-methyl-1-pentene in such an amount as to not change the inherent properties of the copolymer, that is, usually in an amount of up to about  
25 5 mole % based on the total copolymer. The melting points of these EVOH copolymers are generally between about 160°C and 190°C.

EVOH copolymers are normally prepared by copolymerization of ethylene with vinyl acetate, followed by hydrolysis of the vinyl acetate

component to give the vinyl alcohol group. This process is well known in the art.

The solvent for the solution of the present invention is a mixture of tetrahydrofuran (THF) and water. The composition of the solvent will depend in part on the ethylene content of the EVOH copolymer. Generally, as the fraction of copolymerized ethylene in the EVOH increases, less water should be used in the solvent. Preferred solvent composition is defined by formula (I):

$$(I) \quad 65-E \leq H_2O \leq 90-E$$

wherein  $E$  = mole % copolymerized ethylene in the EVOH, and  $H_2O$  = wt % water in the THF/water binary of the solvent.

Formula (I) is approximate. Maximum and minimum water concentrations from about 5 wt% above, to about 5 wt% below, the concentration predicted by formula (I) may be suitable for use in the present invention. For example, for EVOH with 30 mole % ethylene content, formula (I) predicts acceptable solvent with water in the range of 35-60 wt%. Suitable minimum and maximum water concentrations may be in the ranges of about 30-40 wt% and about 55-65 wt%, respectively. Other factors which can influence the solvent concentration are molecular weight and degree of saponification of the EVOH. To the extent that the foregoing predictive formula is approximate, an ordinary skilled practitioner should be able to determine a proper solvent concentration with only little experimentation.

The order of adding ingredients to the solution is not important. In order to assure the concentration of the solvent, it is preferred to mix the water and THF first then add the EVOH to the liquid mixture. The solution is typically prepared by heating and agitating the ingredients for sufficient time to cause the EVOH to dissolve in the solvent. Duration



of heating and extent of agitation will depend on such factors as the operating temperature, concentration of EVOH in solution and form of the EVOH copolymer. EVOH is typically available in form of pellets having maximum dimension of about 3-6 mm. It can be supplied in

5 sheet and slab form which should preferably be comminuted to smaller particles to facilitate dissolving. Waste EVOH film can be recovered for solution coating according to this invention and should be shredded or ground to dissolve more quickly. Typically, the solution ingredients are heated and maintained at an elevated temperature, preferably the

10 solution boiling point, in an agitated vessel until the copolymer has dissolved. Evaporated solvent is condensed and refluxed. If a lower temperature is employed, dissolving will take longer. Preferably, the ingredients should be heated to a temperature of at least 60°C and, more preferably, to a temperature of at least 65°C. The atmospheric

15 boiling points of THF/water solutions of this invention are about 67°C. It is possible to increase the rate of solution by further elevating the temperature. This could be accomplished, for example, by dissolving in a closed system under pressure. The solution should not be heated to such a high temperature that the EVOH thermally degrades. Ordinarily,

20 dissolution should be fast enough for industrial purpose if the dissolution temperature does not exceed 100°C.

The coating solutions of the present invention preferably contain about 8 to about 14 wt% EVOH, and more preferably about 8 to about 12 wt% EVOH. Generally, higher EVOH concentrations produce higher

25 solution viscosities at given temperature and EVOH molecular weight. Consequently, EVOH concentrations higher than about 20 wt% are usually too viscous for application by conventional solution coating equipment and processes. Solutions having less than about 7 wt% EVOH are commercially unattractive because of the cost of excess

solvent; the equipment needed to recover excess solvent; and the tendency to produce excessively hazy and blistered coatings when large volumes of solvent are removed too quickly from wet coatings at commercially preferred drying rates.

- 5        After the solids have been dissolved, the solution can be brought to ambient temperature, either by cooling the solution or by simply removing the source of heat. Alternatively, the solution can be coated onto a substrate at elevated temperature.

- 10       Solutions prepared in accordance with the present invention are typically stable, *i.e.*, they will not gel or precipitate, for at least several days. Agitation can be stopped as soon as the EVOH is dissolved. The coating solution can be transferred to storage facilities or can be used directly after preparation.

- 15       Solutions of this invention can be coated onto substrates by any of the processes well known in the art such as dip coating, knife coating, gravure coating and roll coating. These solutions should find acceptance in coating processes for which low viscosity is important, such as for example, spray coating. Normally, the solution is applied to a surface of a substrate and the solvent is removed. Solvent removal, 20 sometimes hereinafter referred to as drying, can be achieved by subjecting the wet, coated film to high temperature, vacuum or a combination of these for a sufficient time to cause the solvent to evaporate. Preferably drying is accomplished by subjecting the wet-coated substrate to elevated temperature, however, the temperature 25 should not be high enough to degrade the film.

The dry coating can be produced by a single application of the solution to the substrate or, primarily when thicker coatings are desired, the coating thickness can be built up by repeated applications of solution followed by solvent removal. Although the dried, coated films



made by the process of the present invention can be heat treated as is sometimes practiced in the art, it is not necessary to perform such heat treatment to achieve beneficial properties.

Coating solutions according to the present invention can also  
5 include other additives, such as for example, slip additives, which improve the ease of applying the coating solutions to substrates. Some slip additives are organic and may dissolve in the solvent. Normally, slip additives are insoluble inorganic compounds. A preferred slip additive is a mineral mixture now or formerly available from Pfizer  
10 Minerals under the tradename of Talcron® and believed to consist of 61 wt% SiO<sub>2</sub>, 31 wt% MgO and the remainder other metal oxides. When insoluble additives are used, they can be charged to the agitated solution where they remain in suspension until the coating solution is applied to the substrate. Insoluble additives should be of sufficiently  
15 small particle size to resist settling from suspension after agitation is stopped. If suspensions do settle, they can be easily redispersed by further agitation.

The substrate to which solutions of the present invention can be applied are preferably plastics, such as polyester, including for example  
20 polyethylene terephthalate; polyamides, including for example, poly(hexamethylene adipamide) or nylon 6,6, poly( $\epsilon$ -caprolactam) or nylon 6, poly(hexamethylene terephthalamide), nylon 11, nylon 12, and nylon 12,12; cellulose such as regenerated cellulosic film and paper, for example; and metal. Such substrates may themselves be multilayer  
25 composites which include metal or inorganic chemical coatings. EVOH solutions of the present invention can also be applied over adhesive layers, typically known in the industry as "tie layers", for improving the bond between substrate and the EVOH.

EVOH-coated substrates made according to the process of the present invention can be used in packaging applications where a barrier to oxygen is important. Such applications include packaging of oxygen-sensitive materials, such as chemicals, and foods, such as for example, coffee, chocolate, processed meat, cheese, and pet food.

### EXAMPLES

This invention is now illustrated by representative examples of certain preferred embodiments thereof, where all parts, proportions, and percentages are by weight, unless otherwise indicated. All units of weight and measure other than SI units have been converted to SI units. Unless otherwise noted, oxygen transmission rate and permeability value in the examples were measured at 30°C.

#### Examples 1-7 and Comparative Examples C1-C8

In each example, 50 g of fully hydrolyzed, ethylene/vinyl alcohol copolymer was dissolved in 450 g of solvent of deionized water and cosolvent. The EVOH had either 30 mol% ethylene content, and melt flow of 9 dg/min. at 210 °C measured according to ASTM Standard D-1238, or 44 mol% ethylene content and melt flow of 16. The solvent was agitated in a 1 L resin kettle at room temperature while EVOH pellets were charged. The mixture was then gradually heated to boiling and maintained at boiling with agitation for 2 hours. Thereafter, while agitation was maintained, heat was removed which allowed the solution to cool to room temperature, i.e., 19-21°C, overnight. Viscosity of the solution was measured with a model LV, Brookfield viscometer. The solution was stored at room temperature in closed jars without agitation and appearance was determined periodically by visual inspection. Formation of dispersion was readily observed by loss of clarity and

deposition of particles on the wall of the jar. Shelf life was the number of storage days until dispersion was observed.

Operating conditions and results are summarized in Table I. THF composition in solvent was generally from about 45 wt% to about 5 70 wt% and the upper and lower limits depended slightly on composition of the EVOH. Viscosities of the operative examples were consistently lower than those of solutions with isopropyl alcohol cosolvent, which is recognized in the art as a solvent for EVOH. Shelf life of the THF/water solutions were also longer than the isopropyl 10 alcohol cosolvent examples.

Table I

Example No.	Ethylene in EVOH Wt%	Wt% EVOH in Solution	Co-Solvent	Wt% Water in Solvent	Brookfield Viscosity Pa.s	Shelf life Days
1	30	10	THF	53	0.131	5-15
2	30	10	THF	43	0.123	10-20
3	30	10	THF	38	0.145	10-20
4	30	10	THF	38	0.125	10-20
C1	30	10	THF	72	*	0
C2	30	10	THF	63	*	0
C3	30	10	THF	33	*	0
C4	30	10	IPA	45	0.202	1-2
C5	30	10	IPA	55	0.218	1-2
5	44	10	THF	25	0.141	3-5
6	44	10	THF	33	-	3-5
7	44	10	THF	40	0.158	2-4
C5	44	10	THF	15	**	0
C6	44	10	THF	50	**	0
C7	44	10	IPA	33	**	0
C8	44	10	IPA	45	**	0

\* = Formed Two Phases

\*\* = Gelled

Examples 8-11 and Comparative Example C9

EVOH/THF/Water solutions were prepared using the materials and procedures of Example 1. Proportions of ingredients and results of tests described below are summarized in Table II. After the solutions

5 had cooled to room temperature, they were cast onto 23  $\mu\text{m}$  thick, polyethylene terephthalate (PET) film, using a coating knife with a 100  $\mu\text{m}$  gap. Within about 10 seconds of coating, the films were placed for 1 minute in a convection oven at 100°C to dry. Haze value was

10 measured with a HunterLab ColorQuest Sphere Spectrocolorimeter (version 3.2).

Table II

Example No.	Ethylene in EVOH W%	Wt% EVOH in Solution	Co-Solvent	Wt% Water in Solvent	Coating		Haze %
					g/m <sup>2</sup>	Thickness $\mu$ m	
8	30	8	THF	35	7.4	6.2	13.3
9	30	10	THF	35	2.1	1.8	12.0
10	30	12	THF	35	7.1	5.9	11.0
11	30	14	THF	35	3.8	3.2	11.4
C9	30	6	THF	35	1.2	1.0	64.4

Example 12

An EVOH copolymer of 30 mol% ethylene and 37 dg/min. melt flow was prepared to provide low viscosity in solution. A 10.5% solids solution was made by dissolving 50 g of this copolymer in a mixture of 200 g THF and 225 g deionized water in the manner of Example 1. The solution was cast onto a 23  $\mu\text{m}$  thick PET film as in Example 8 to produce a 2.1  $\mu\text{m}$  dried coating thickness which exhibited excellent clarity and appearance.

Oxygen permeability of the coated film was measured at both 35% and 80% relative humidity as 9 and 29  $\text{mL}/\text{m}^2\cdot\text{day}\cdot\text{atm}$ , respectively. After correction for the known oxygen permeability of uncoated PET film (i.e., 70  $\text{mL}/\text{m}^2\cdot\text{day}\cdot\text{atm}$ ) and film thickness were made, the oxygen permeability of the unit thickness EVOH layer was calculated as 10 and 113  $\text{mL}\cdot\mu\text{m}/\text{m}^2\cdot\text{day}\cdot\text{atm}$  at 35% and 80% relative humidity, respectively. Such values are considered excellent at 30°C.

Example 13

The procedure of Example 5 was repeated using 50 g of EVOH copolymer with 44 mole % copolymerized ethylene content and melt flow of 16 dg/min., to make a 10 wt% solids solution in 75 wt% THF/25 wt% water solvent. The solution, which remained clear after cooling to room temperature, was cast onto 23  $\mu\text{m}$  thick, PET film with a 50  $\mu\text{m}$  gap coating knife, then dried in a 110°C oven for 2 minutes to form a dried coating of 1.75  $\mu\text{m}$  thickness. Oxygen permeability for the coated film was measured as 27 and 39  $\text{mL}/\text{m}^2\cdot\text{day}\cdot\text{atm}$  at 44% and 80% relative humidity, respectively.

Examples 14-16 and Comparative Examples C10-C12

Coating solutions of the EVOH of Example 1 were prepared in 62 wt% THF/38 wt% water solvent. A 9.7 wt% solids solution ("solution A") was made by adding 247.7 g EVOH to 1625 mL THF and 875 mL water



in an agitated 4 L resin kettle. The mixture was heated to boiling and after the polymer had dissolved, 2.3 g of Pfizer Minerals Talcron® additive was charged then the solution was cooled to room temperature (about 25°C). A 6.0 wt% solids solution ("solution B") was prepared by  
5 the same procedure except that 2732 mL of THF and 1488 mL of water were used.

The solutions were coated onto one side of a 12  $\mu\text{m}$  thick and 280 mm wide, PET film using a 28 cm wide, continuous doctor roll coating system (1) shown in the Figure. The film (2) was pulled from  
10 supply roll (4) and redirected by roll (6). The film was pulled in the gap (8) between two, 6.35 cm diameter, counter-rotating rolls (10) and (12) turning at the same surface velocity as the film speed. A pan (14) containing the coating solution (16) was placed beneath roll (12) to partially immerse the roll and causing it to apply coating solution at  
15 room temperature to one side of the film. The coating thickness was determined by the size of the gap. The coated film was then passed through a 2.3 m long, hot air convection drier (18), heated by means not shown, in which solvent was removed. The dried film was wound up outside the drier with directional rollers (20), (22) and (24), and  
20 wind-up roller (26), then tested for haze, residual THF content and oxygen barrier properties. Rollers (10), (12) and (26) were driven in the directions indicated by the arrows, by conventional means not shown. Operating conditions and test results are summarized in Table III.

TABLE III

Example No.	Solids in solution Wt%	Film Speed m/s	Drying		Coating Thickness $\mu\text{m}$	Haze (%)	OTR (1)		OPV (2)	
			Time Sec.	Temp. Avg. $^{\circ}\text{C}$			40% RH	80% RH	40% RH	80% RH
14	9.7	0.18	13	119	2.2	8.7	6.0	28.8	14	80
15	9.7	0.41	6	119	2.9	8.4	6.2	36.7	18	141
16	9.7	0.20	11	103	2.6	8.2	6.8	34.1	17	106
C10	6.0	0.18	13	116	2.0	42.8	12.4	42.7	27	123
C11	6.0	0.25	9	115	1.9	42.5	16.3	54.8	35	173
C12	6.0	0.38	6	100	1.2	60.2	16.2	70.1	23	176

(1) Coated-film oxygen transmission rate  $\text{mL}/\text{m}^2\cdot\text{day}\cdot\text{atm}$  at 40% and 80% relative humidity (RH)

(2) EVOH oxygen permeability value,  $\text{mL}\cdot\mu\text{m}/\text{m}^2\cdot\text{day}\cdot\text{atm}$  at 40% and 80% RH

(3) Hunterlab ColorQuest Sphere Spectro-Colorimeter, Version 3.2

Films of this invention were much clearer and appeared better than the comparative films which had higher haze levels and many very small surface blisters observed by visual inspection. Barrier properties of the films according to this invention were also better than the comparative example films. At both 40% and 80% relative humidity, the comparative films had higher oxygen transmission rates (OTR). Oxygen permeation values (OPV) for unit thickness of coating were calculated using an OTR value of  $140 \text{ mL/m}^2 \cdot \text{day} \cdot \text{atm}$  for the uncoated, PET film. OPV of operative example coatings were universally lower than the comparative coatings except that at 80% relative humidity, Example 15 OPV ( $141 \text{ mL} \cdot \mu\text{m/m}^2 \cdot \text{day} \cdot \text{atm}$ ) exceeded the OPV of Example C10 ( $123 \text{ mL} \cdot \mu\text{m/m}^2 \cdot \text{day} \cdot \text{atm}$ ). These results are believed attributable to the combination of drying time and temperature and coating thickness conditions. More specifically, relative to C10, Example 15 had much shorter drying time at about the same drying temperature, and greater coating thickness. Residual THF of less than  $150 \text{ mg/m}^2$  was measured in the dried coatings. Such amounts should not detract from the usefulness of coated films of this invention.

#### 20 Example 17

A surface of a  $23 \mu\text{m}$  thick PET film was primed with about  $0.3 \mu\text{m}$  adhesive layer of ethylene/vinyl acetate copolymer containing 28% vinyl acetate and grafted with 0.3% maleic anhydride. The adhesive was coated from a 12% solution in 50/50 toluene/THF solvent by a gravure method using a No. 110 quad-cell cylinder and convection air oven drying at  $107^\circ\text{C}$ . The primed film was top-coated with solution A according to the procedure of Example 12, except that coating speed was  $0.18 \text{ m/s}$ , average drier air temperature was  $118^\circ\text{C}$  and drying time was 13 seconds. A dry EVOH coating of  $1.7 \mu\text{m}$  thickness, having

good appearance and 18% haze was obtained. The EVOH side of a strip of coated film was laminated to a pressure sensitive tape. The tape and film were subjected to a "T" peel strength test at 2 cm/min. which indicated good adhesion between the EVOH and PET substrate of 20 g/cm.

#### Example 18

A 2.6  $\mu\text{m}$  dry thickness top layer was coated on the aluminum surface layer of a metallized-PET film (DuPont Mylar® 48MM20) using solution A according to the procedure of Example 12 except that coating speed was 0.25 m/s, average drier air temperature was 115°C and drying time was 9 seconds. The OTR at 80% relative humidity improved from 2.8 mL/m<sup>2</sup>•day•atm for the uncoated, metallized-film to 0.84 mL/m<sup>2</sup>•day•atm for the EVOH-coated film. Both uncoated and coated films were subjected to Gelbo flexing for 10 cycles after which oxygen transmission rate was again measured. The OTR of the EVOH-coated film only deteriorated by a factor of 3.2 to 2.7 mL/m<sup>2</sup>•day•atm while the uncoated, metallized-film rate deteriorated 7.4 times to 20.8 mL/m<sup>2</sup>•day•atm.

#### Example 19

Solution A was applied to one surface of a 20  $\mu\text{m}$  thick, nylon film available under the tradename "Dartek"-130. The procedure of Example 12 was used with coating speed of 0.25 m/s, average drier air temperature of 115°C and drying time of 9 seconds to produce a dry coating of 2.3  $\mu\text{m}$  thickness.

The oxygen transmission rates of the coated nylon film at 42% and 80% relative humidity were 4.5 and 33 mL/m<sup>2</sup>•day•atm, respectively. By comparison, the transmission rates for the uncoated nylon film were 40 and 82 mL/m<sup>2</sup>•day•atm, respectively. The oxygen

permeability values of the EVOH layer at 42% and 80% relative humidity were calculated to be 11 and 110 mL• $\mu$ m/m<sup>2</sup>•day•atm, respectively.

I claim:

1. A process for solution coating a substrate with an ethylene/vinyl alcohol copolymer (EVOH) barrier, comprising the steps of:

5 (1) agitating a coating solution consisting essentially of  
(A) about 7 to about 20 wt% ethylene/vinyl alcohol copolymer having copolymerized ethylene content from about 20 to about 55 mole %; and

10 (B) a complementary amount to total to 100 wt% of a solvent consisting essentially of about 10 to about 70 wt% water; and a complementary amount to total 100 wt% of tetrahydrofuran;

at a temperature within the range of about 55-100°C until a clear solution is obtained;

15 (2) coating at least one surface of the substrate with the coating solution; and

3) removing the solvent, whereby a dry ethylene/vinyl alcohol copolymer coating on the at least one surface is produced.

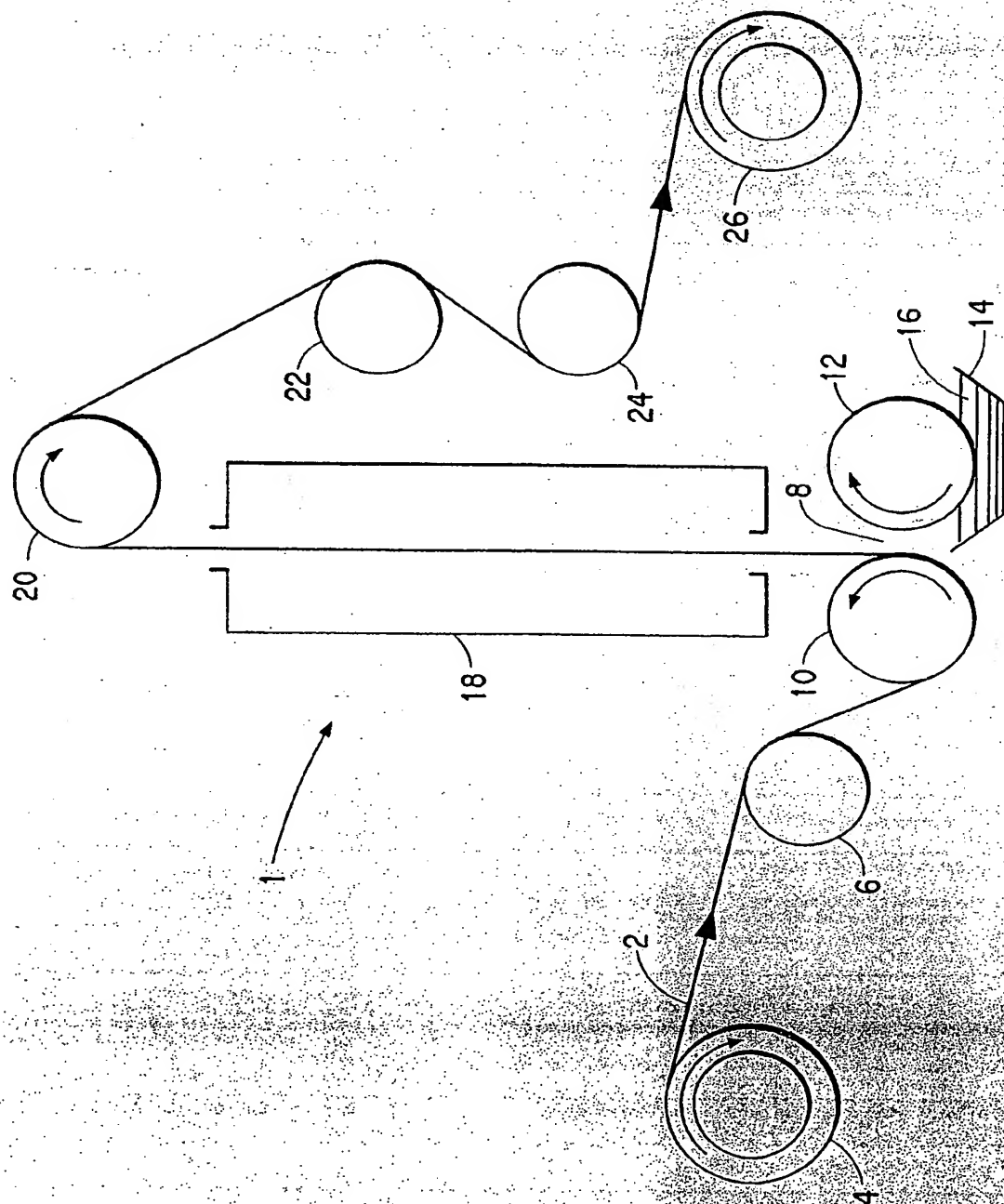
20 2. A process of claim 1 wherein the ethylene/vinyl alcohol copolymer is about 8 to about 14 wt% of the coating solution.

25 3. A process of claim 1 wherein the solvent consists essentially of water present in weight percent concentration of at least about 65 minus the mole percent copolymerized ethylene content of the ethylene/vinyl alcohol copolymer, and at most about 90 minus the mole percent copolymerized ethylene content of the ethylene/vinyl alcohol copolymer; and a complementary amount to total to 100 weight percent of tetrahydrofuran.

4. A process of claim 1 wherein the at least one surface of the substrate is selected from the group consisting of polyester, polyamide, regenerated cellulosic film, metal-coated polyester and paper.
5. A process of claim 4 wherein the polyester is polyethylene terephthalate.
6. A coating solution consisting essentially of:
  - (A) about 7. to about 20 wt% ethylene/vinyl alcohol copolymer having copolymerized ethylene content from about 20 to about 55 mole %; and
  - 10 (B) a complementary amount to total 100 wt% of a solvent consisting essentially of about 10 to about 70 wt% water; and a complementary amount to total 100 wt%, of tetrahydrofuran.
7. A coating solution of claim 6 wherein the ethylene/vinyl alcohol copolymer is about 8 to about 14 wt% of the coating solution, and  
15 wherein the solvent consists essentially of water present in weight percent concentration of at least about 65 minus the mole percent copolymerized ethylene content of the ethylene/vinyl alcohol copolymer, and at most about 90 minus the mole percent copolymerized ethylene content of the ethylene/vinyl alcohol  
20 copolymer; and a complementary amount to total to 100 weight percent of tetrahydrofuran.
8. A coated film made by the process of claim 1.



FIGURE



## INTERNATIONAL SEARCH REPORT

International application No.  
PCT/US 94/09462

## A. CLASSIFICATION OF SUBJECT MATTER

IPC 6 C08J7/04 C09D129/04 C08J3/09

According to International Patent Classification (IPC) or to both national classification and IPC

## B. FIELDS SEARCHED

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IPC 6 C08J C09J C09D C08L

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

## C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X A	GB,A,2 138 350 (TOYO SEIKAN KAISHA LTD) 24 October 1984  see claims 1,2 see page 2, line 127 - page 3, line 27 ----	8  1,4-6
X A	EP,A,0 465 912 (MOPLEFAN S.P.A.) 15 January 1992  see claims 1-5 -----	8  1,6

☐ Further documents are listed in the continuation of box C.

☒ Patent family members are listed in annex.

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Date of the actual completion of the international search

2 December 1994

Date of mailing of the international search report

30.12.94

Name and mailing address of the ISA

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# INTERNATIONAL SEARCH REPORT

Information on patent family members

International application No.  
PCT/US 94/09462

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
GB-A-2138350	24-10-84	JP-C- 1483731	27-02-89
		JP-A- 59158232	07-09-84
		JP-B- 63030132	16-06-88
		SE-B- 463755	21-01-91
		SE-A- 8401063	29-08-84
		US-A- 4517274	14-05-85
		US-A- 4534930	13-08-85
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EP-A-0465912	15-01-92	NONE	
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